



# Application of the Reciprocal Rate Index Analysis Method to Section 4 Tests

IPS-5.3-22

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- Radial flow test for CFE
  - Data reduction approach given in API RP 19B
  - Application Example
- Axial flow test for PR
  - Data reduction approach given in API RP 19B
  - Application Example
- The viscosity-corrected reciprocal rate index approach
  - Application and assessment
- So what?

- Sandstone core
- Deep penetrating charge
- Axi-radial pressure/flow configuration
- Production-direction gas flow
- 70 °F Post-Shot Flow
- Core Flow Efficiency metric (CFE) used to evaluate flow performance

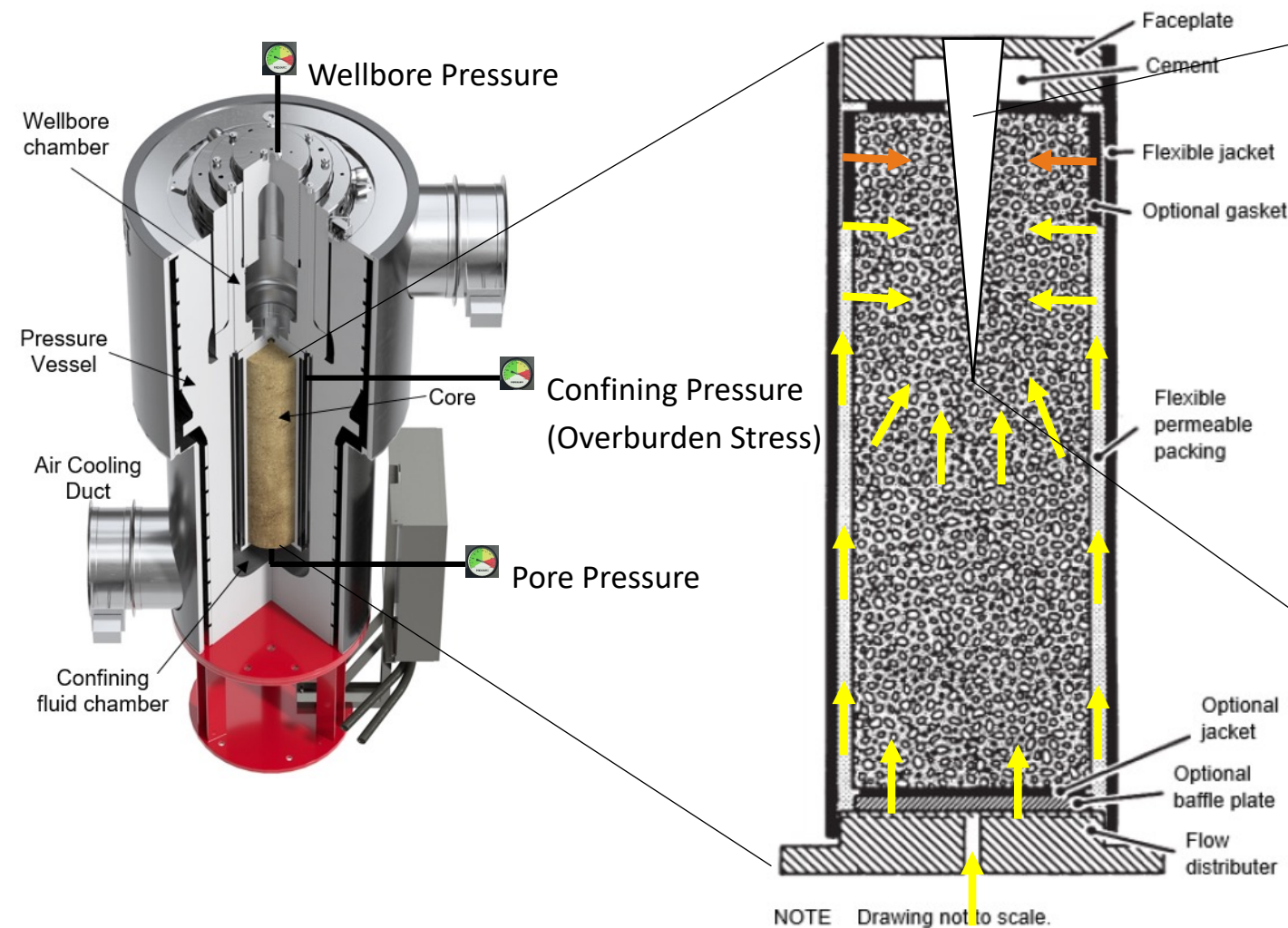
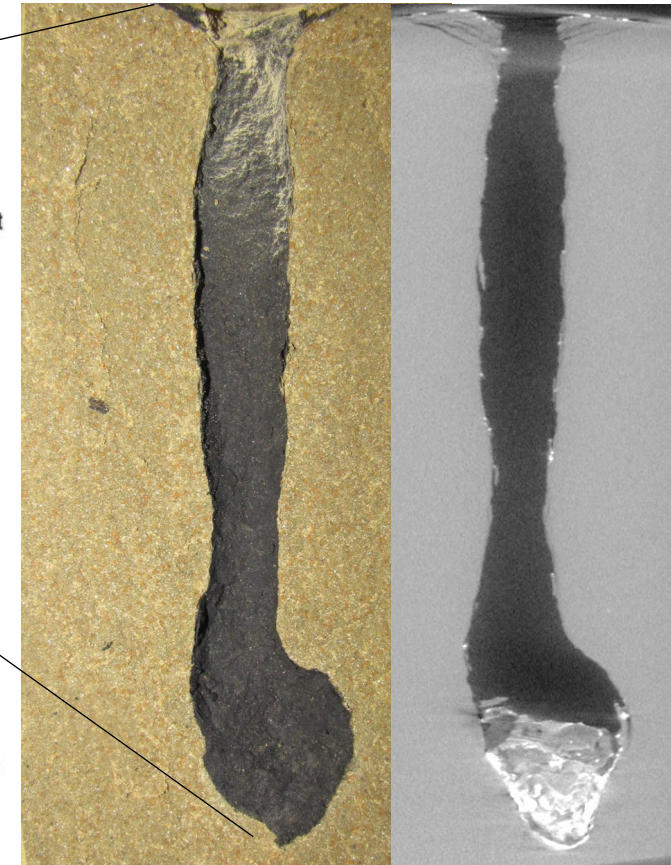


Figure 10—Typical Radial-flow Geometry



## Gas Flow Data Reduction (API 2021)

- 4.4.11.5 Core Flow Efficiency: CFE shall be defined according to Eqn(16):

$$CFE(Q_m) = \frac{PI_{actual}}{PI_{ideal}} = 5.79 \times 10^6 \times \frac{\left( \frac{\mu}{2k_h \beta \pi D_{op}} \ln \left( \frac{R_{core}}{R_{tunnel}} \right) + \frac{c_f Q_m}{\sqrt{k_h} \beta (2\pi L)^2 L_{eff}} \right)}{a_{1,actual} + a_{2,actual} Q_m}$$

- Eqn(16) assumes

- The ordinary differential equation
 
$$-\frac{dp}{dR} = \frac{\mu}{k} \left( \frac{Q_m}{\rho A} \right) + \frac{c_f \rho}{\sqrt{k}} \left( \frac{Q_m}{\rho A} \right)^2$$

- The radial flow model,  $A = 2\pi R L_p$ ; no hemispherical cap flow
- Ideal gas law
- $PI = Q_m / (\bar{p} \Delta p)$

- After integration:

- $\bar{p} \Delta p = \frac{\mu Q_m}{2\pi \beta k L_p} \ln \left( \frac{R_{core}}{R_{tunnel}} \right) + \frac{c_f}{\sqrt{k} \beta} \frac{Q_m^2}{(2\pi L_p)^2 L_{eff}}$

- $a_1 = \frac{\mu}{2\pi \beta k L_p} \ln \left( \frac{R_{core}}{R_{tunnel}} \right); a_2 = \frac{c_f}{\sqrt{k} \beta (2\pi L_p)^2 L_{eff}}$

- $\bar{p} \Delta p = a_1 Q_m + a_2 Q_m^2$ 
  - This is a two-term 2<sup>nd</sup>-order polynomial

## Gas Flow Data Reduction (API 2021)

- 4.4.11.5 Core Flow Efficiency: CFE shall be defined according to Eqn(16):

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- $\bar{p}\Delta p = Q_m(a_1 + a_2 Q_m)$

- Eqn(16) has the form:

$$CFE(Q_m) = \left( \frac{Q_m}{\bar{p}\Delta p} \right)_{actual} \cdot \left( \frac{\bar{p}\Delta p}{Q_m} \right)_{ideal}$$

$$= \frac{(\bar{p}\Delta p)_{ideal}}{(\bar{p}\Delta p)_{actual}} \Big|_{Q_m}$$

$$= \frac{[Q_m(a_1 + a_2 Q_m)]_{ideal}}{[Q_m(a_1 + a_2 Q_m)]_{actual}}$$

$$= \frac{a_{1,ideal} + a_{2,ideal} Q_m}{a_{1,actual} + a_{2,actual} Q_m}$$

## Gas Flow Data Reduction (API 2021)

- Evaluation of  $a_1$  and  $a_2$  for radial flow requires fitting a quadratic curve to a plot of the average pressure times the pressure difference vs. the mass flow rate as shown in Figure 14.

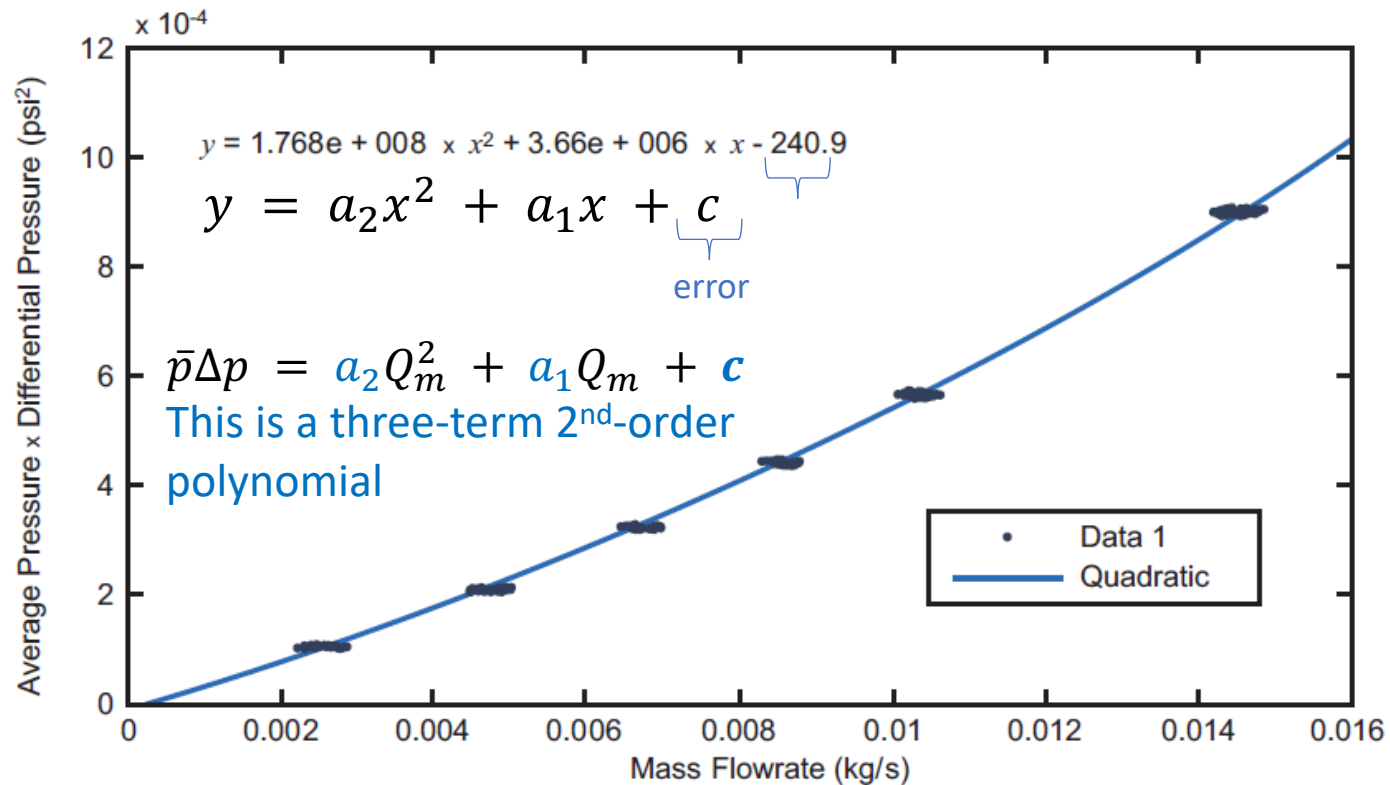


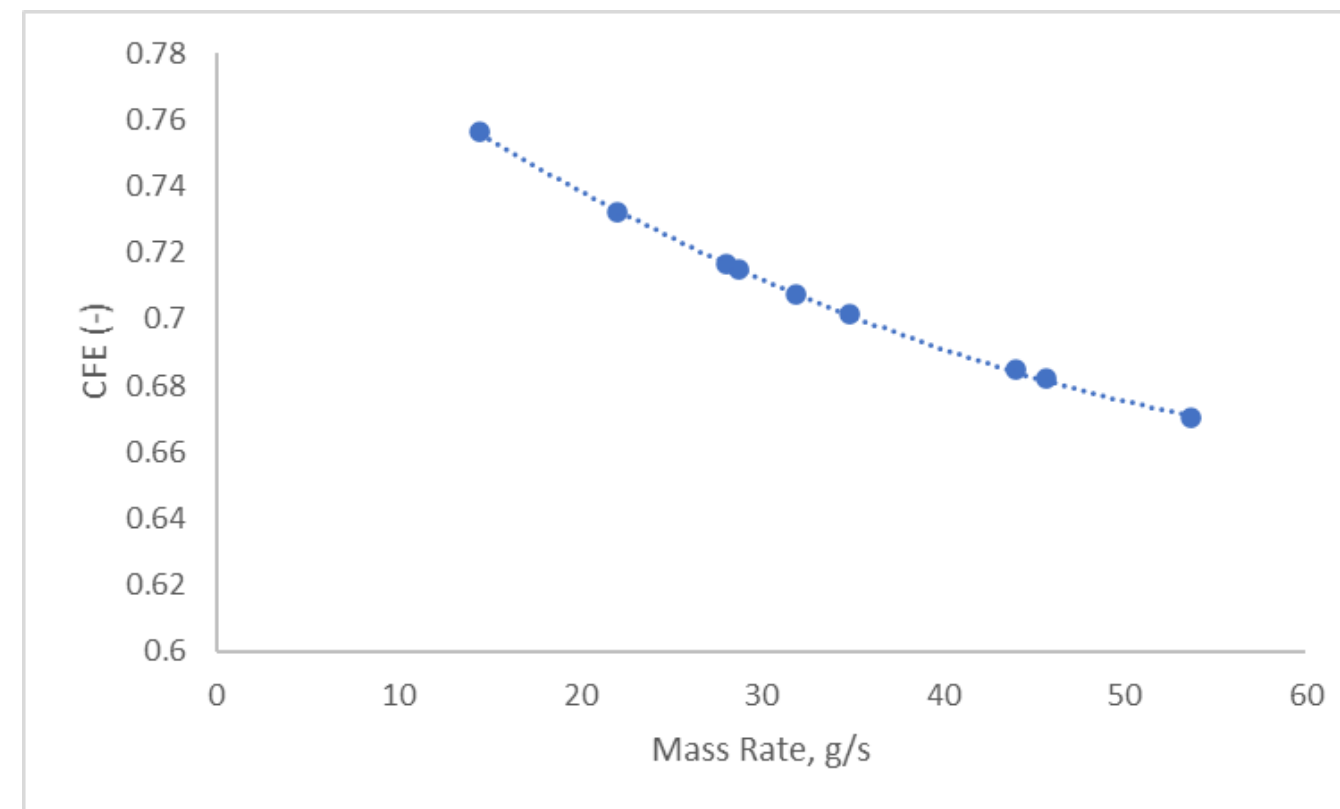
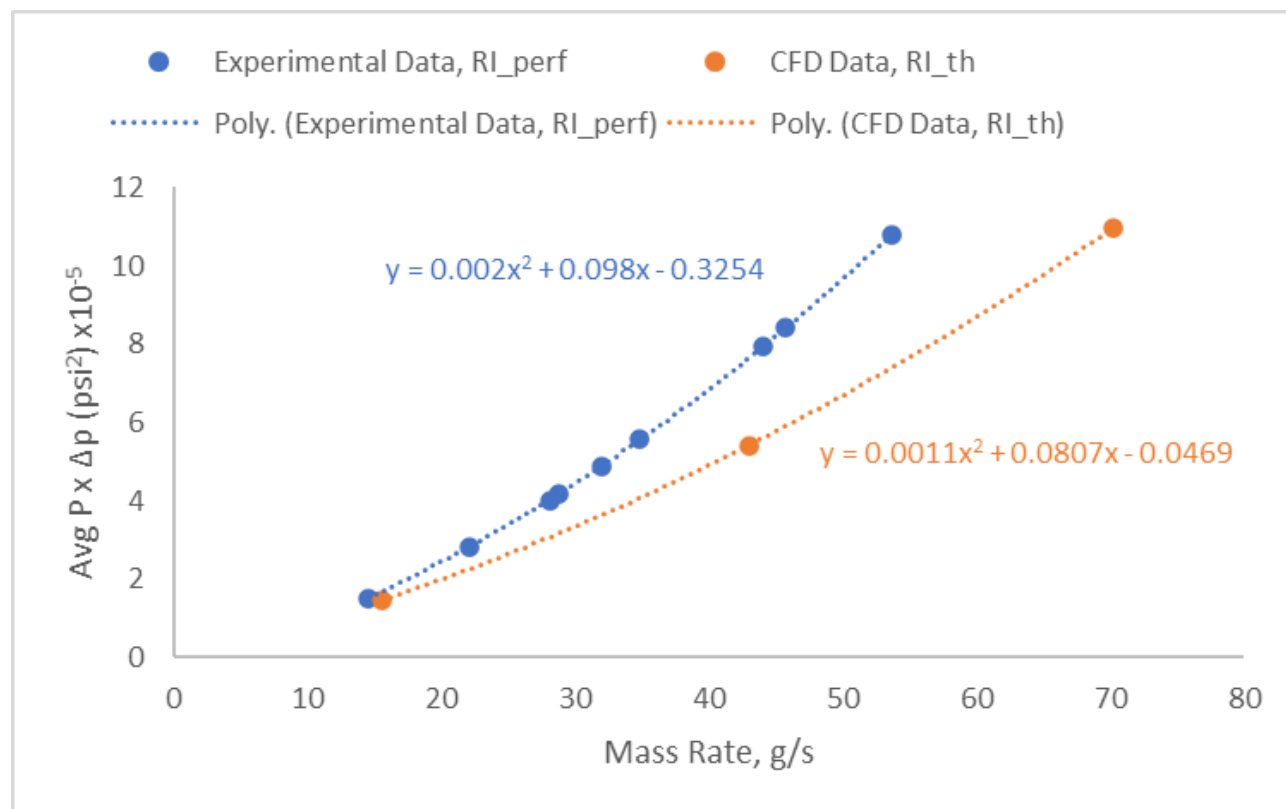
Figure 14—Post-Shot Radial Flow for a Gas Saturated Core

- 4.4.11.5 Core Flow Efficiency: CFE shall be defined according to Eqn(16):

$$CFE(Q_m) = \frac{PI_{actual}}{PI_{ideal}} = 5.79 \times 10^6 \times \frac{\left( \frac{\mu}{2k_h \beta \pi D_{op}} \ln \left( \frac{R_{core}}{R_{tunnel}} \right) + \frac{c_f}{\sqrt{k_h} \beta (2\pi L)^2 L_{eff}} Q_m \right)}{a_{1,actual} + a_{2,actual} Q_m}$$

$$CFE(Q_m) = \frac{[a_1 + a_2 Q_m]_{ideal}}{[a_1 + a_2 Q_m + c]_{actual}}$$

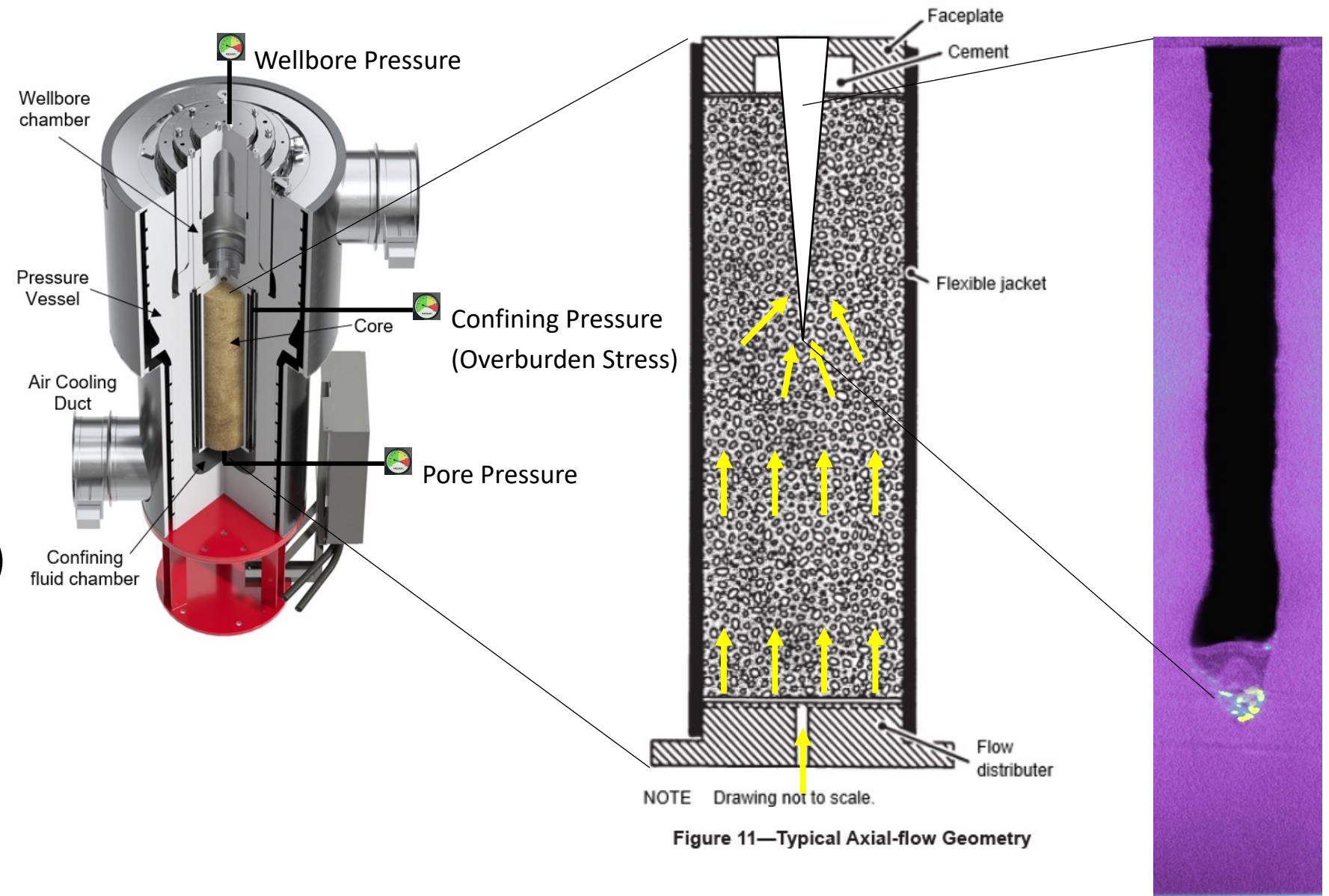
- Regress a three-term 2<sup>nd</sup>-order polynomial to the data and use two of the three coefficients in a two-term 1<sup>st</sup>-order polynomial.



$$CFE(Q_m) = \frac{0.081 + 0.001Q_m}{0.098 + 0.002Q_m}$$

CFE ranges between 0.756 to 0.67 for the range of experimental flow rates tested (14.49 to 53.67 g/s).

- Sandstone core conditioned to  $S_{wr}$
- Deep penetrating charge
- Axial pressure/flow configuration
- Production-direction gas flow
- Pre-Shot Flow at 80 °F ( $\bar{T}_f = 59$  °F)
- Post-Shot Flow at 347 °F ( $\bar{T}_f = 224$  °F)
- Production Ratio metric (PR) used to evaluate flow performance





## Gas Flow Data Reduction (API 2021)

- 4.4.11.4 Production Ratio: Gas flow axial production ratio shall be defined as the ratio of the  $PI_{perf}$  to the pre-shot  $PI$  of the target, calculated according to Equation (15):

$$PR = \frac{PI_{perf}}{PI}$$

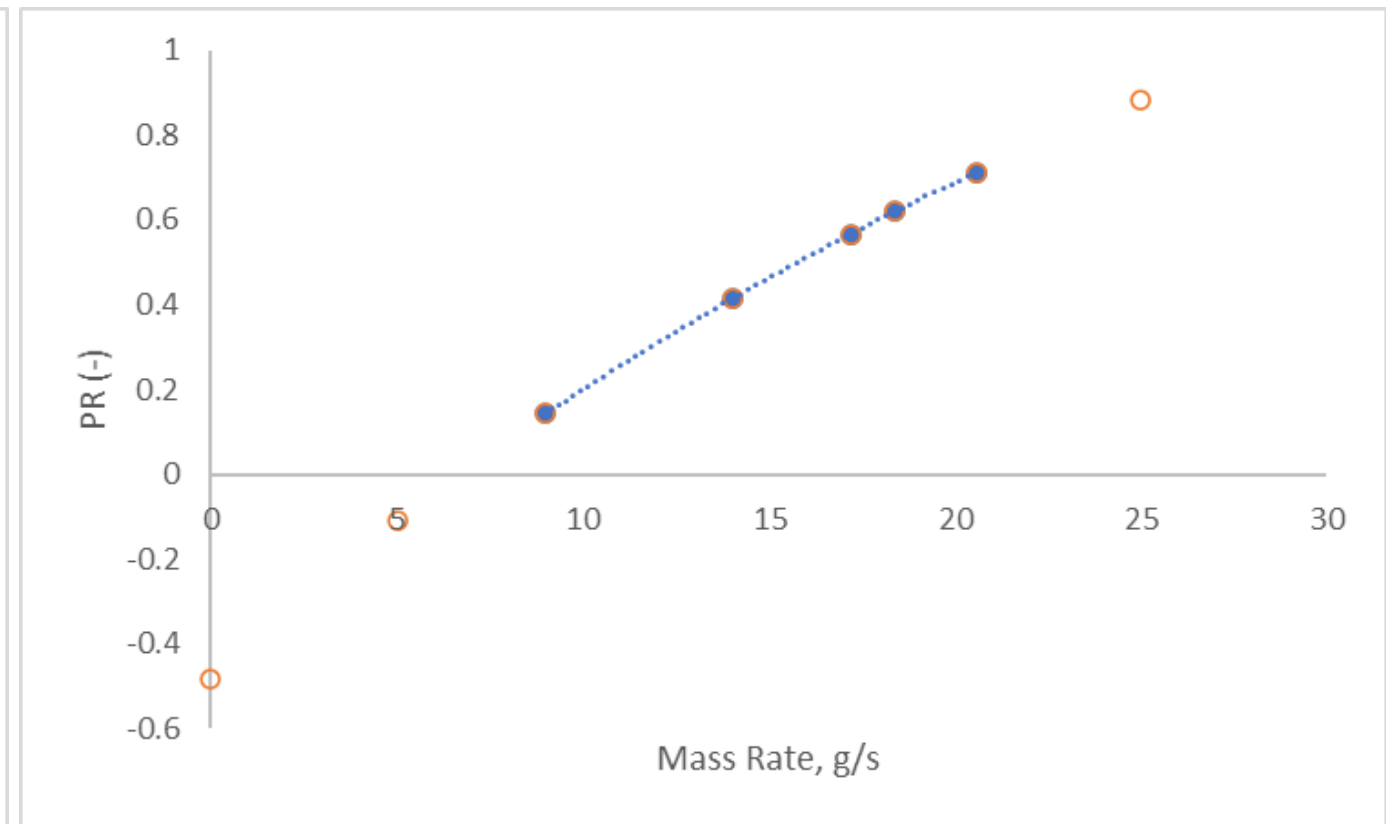
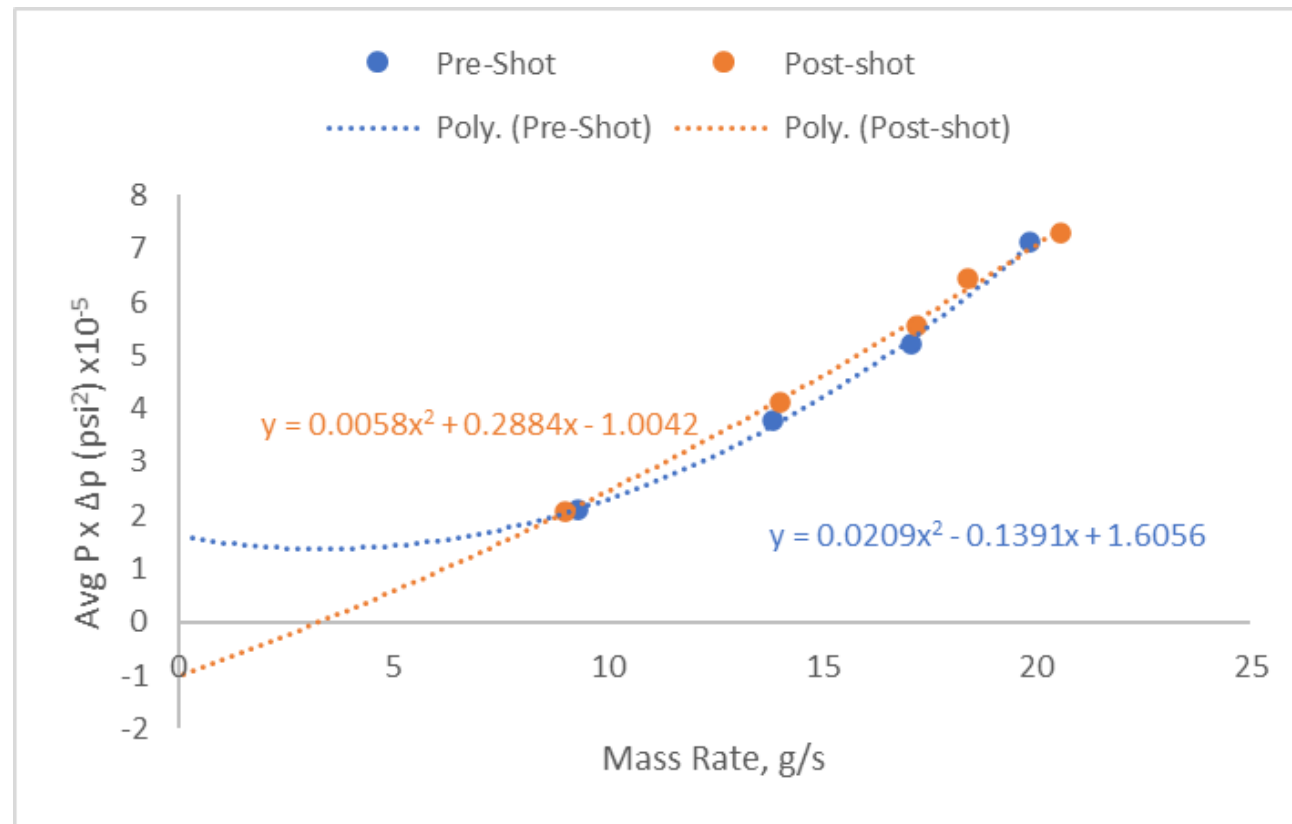
- The method for determining  $PI$  for axial flow is not explicitly given.
- What if we use the same methodology as is given for Core Flow Efficiency?

$$PR(Q_m) = \left( \frac{Q_m}{\bar{p}\Delta p} \right)_{perf} \cdot \left( \frac{\bar{p}\Delta p}{Q_m} \right)_{preshot}$$

$$= \frac{(\bar{p}\Delta p)_{preshot}}{(\bar{p}\Delta p)_{perf}} \Big|_{Q_m}$$

$$= \frac{[a_1 + a_2 Q_m + e]_{preshot}}{[a_1 + a_2 Q_m + e]_{perf}}$$

- No analytical expression for coefficients  $a_1$  and  $a_2$



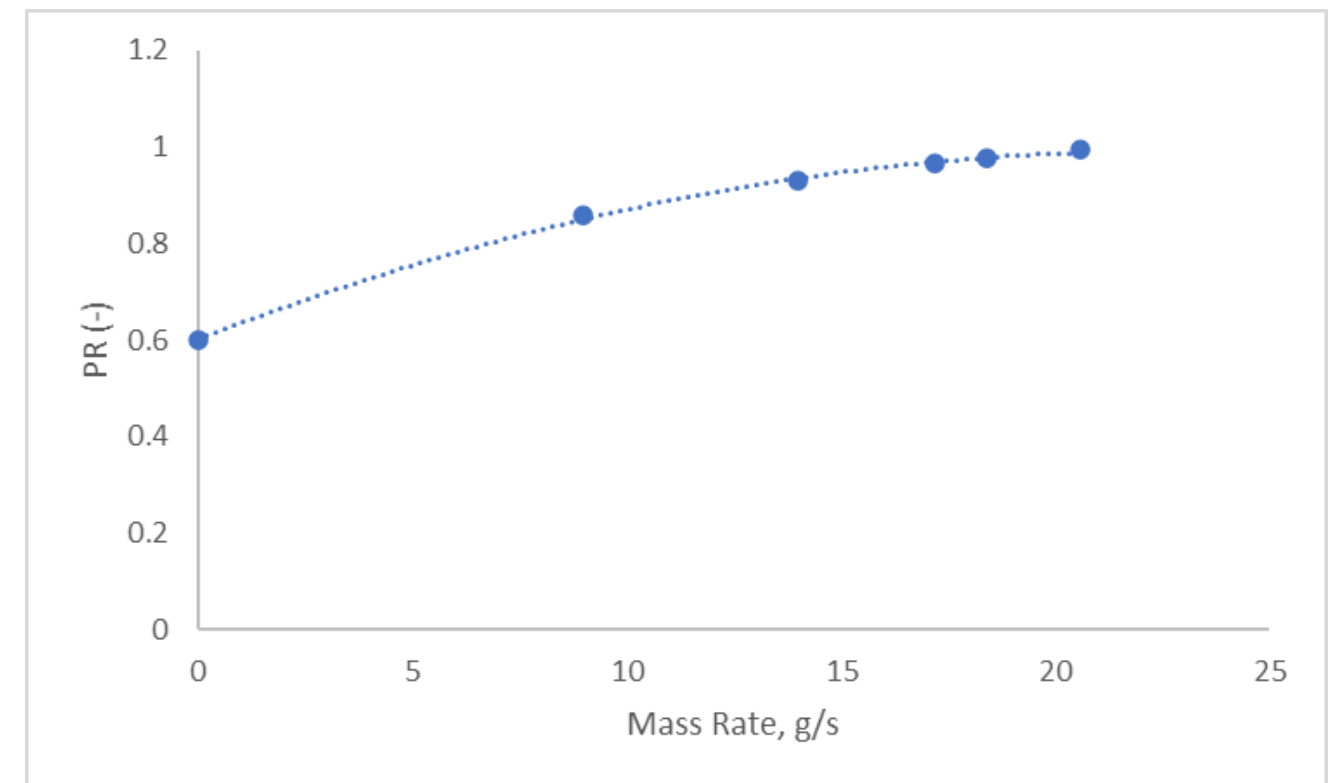
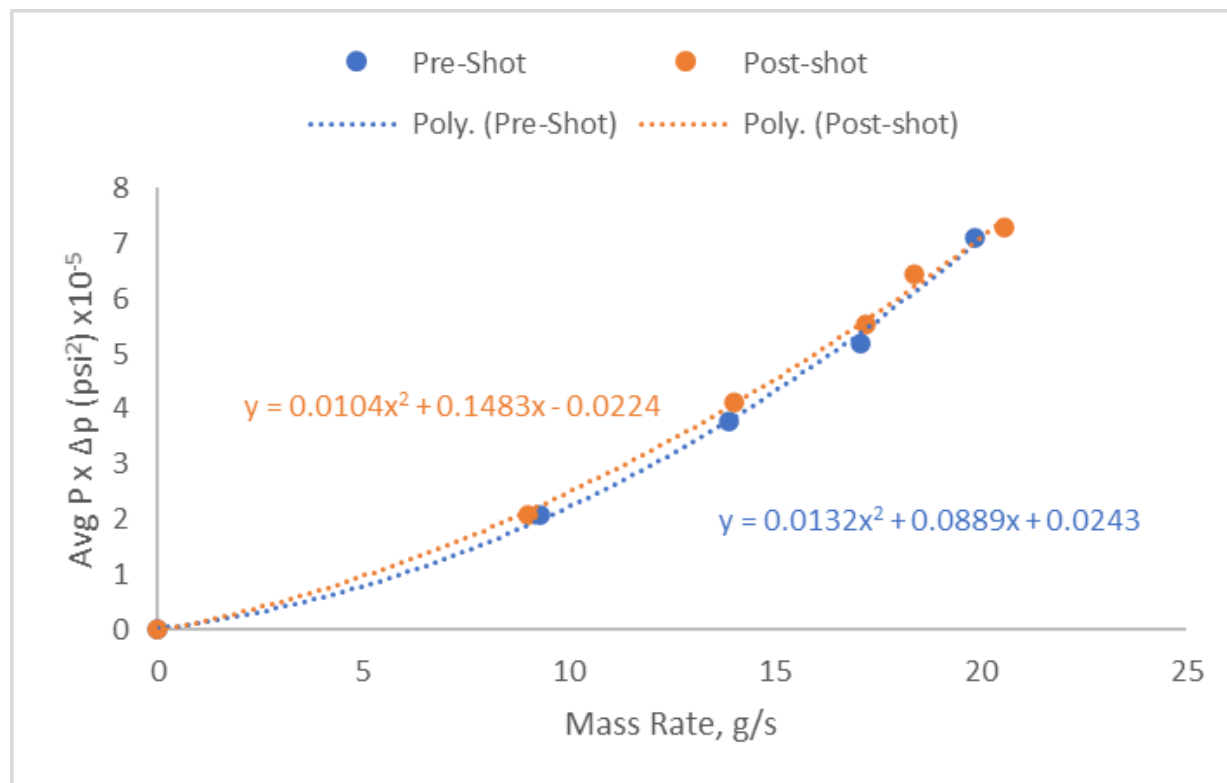
$$PR(Q_m) = \frac{-0.1391 + 0.0209Q_m}{0.2884 + 0.0058Q_m}$$

PR ranges between 0.14 to 0.71 for the range of experimental flow rates tested (9.00 to 20.56 g/s).

- Remedies:
  - Measure  $Q_m$  and  $\bar{p}\Delta p$  at 'zero' (0), and include data in regression analysis

$$PR(Q_m) = \frac{0.0889 + 0.0132Q_m}{0.1483 + 0.0104Q_m}$$

PR ranges between 0.59 to 0.99 for the range of flow rates (0 to 20.56 g/s).

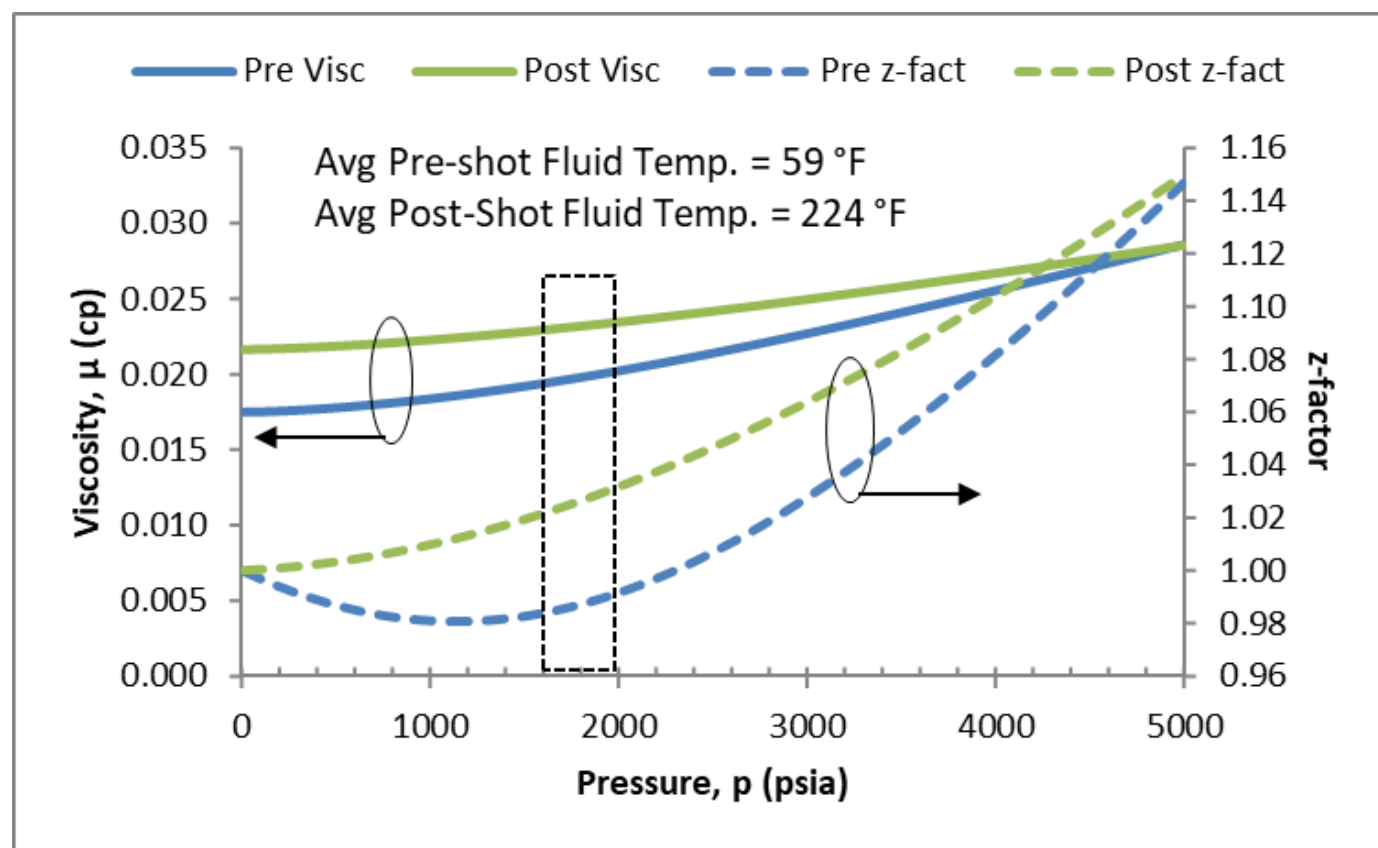


- Recall for this axial flow test,
  - Pre-Shot Flow at 80 °F ( $\bar{T}_f = 59$  °F)
  - Post-Shot Flow at 347 °F ( $\bar{T}_f = 224$  °F)
- Rate Ratio =  $\frac{RI_{perf}(347\text{ °F})}{RI_{preshot}(80\text{ °F})}$ 
  - gas viscosity and density change due to temperature change; essentially two different fluids are being tested.

### For Gas and Liquid Flow Data Reduction

- It would be nice to exclude fluid properties and non-Darcy flow effect from  $RI$ 
  - Recall,  $a_2$  &  $a_1$  are functions of  $p$  &  $T$  since they include  $\mu$  &  $\beta(\rho)$ 
    - $\rho_g(p, T) = pM_w / (z(p, T)RT)$
- It would be nice to have a single value for  $RI$ ,  $RR$ , &  $CFE$  just like we do for the liquid (Darcy) flow tests.

\*Rate Index ( $RI$ ) is generic term for productivity index ( $PI$ ) and injectivity index ( $II$ ).



- Use non-Darcy equation of the form\*:

$$\frac{\Delta m(p)}{q_{sc}\mu_n B_n} = A_1 + A_2 Q_m;$$

$$m(p) = \mu_n B_n \int_{p_b}^p \frac{1}{\mu B} dp + p_b$$

$$B = \rho_{sc}/\rho$$

- When  $\rho$  and  $\mu$  approximately constant,

$$\Delta m(p) \approx \Delta p$$

$$\frac{\Delta p}{q\mu} = A_1 + A_2 Q_m$$

- $A_1$  is only a function of permeability and flow path (length, area, & geometry); is equal to the reciprocal rate index ( $RRI$ ).
- Analytical expressions for  $A_1$  and  $A_2$  can be derived (e.g., for full-face axial-, cylindrical-radial-, and hemispherical-flow).
- $A_1$  (the  $RRI$  value) is determined using a least-squares linear regression.

$$RRI \equiv \lim_{Q_m \rightarrow 0} \left( \frac{\Delta m(p)}{q_{sc}\mu_n B_n} \right) = A_1$$

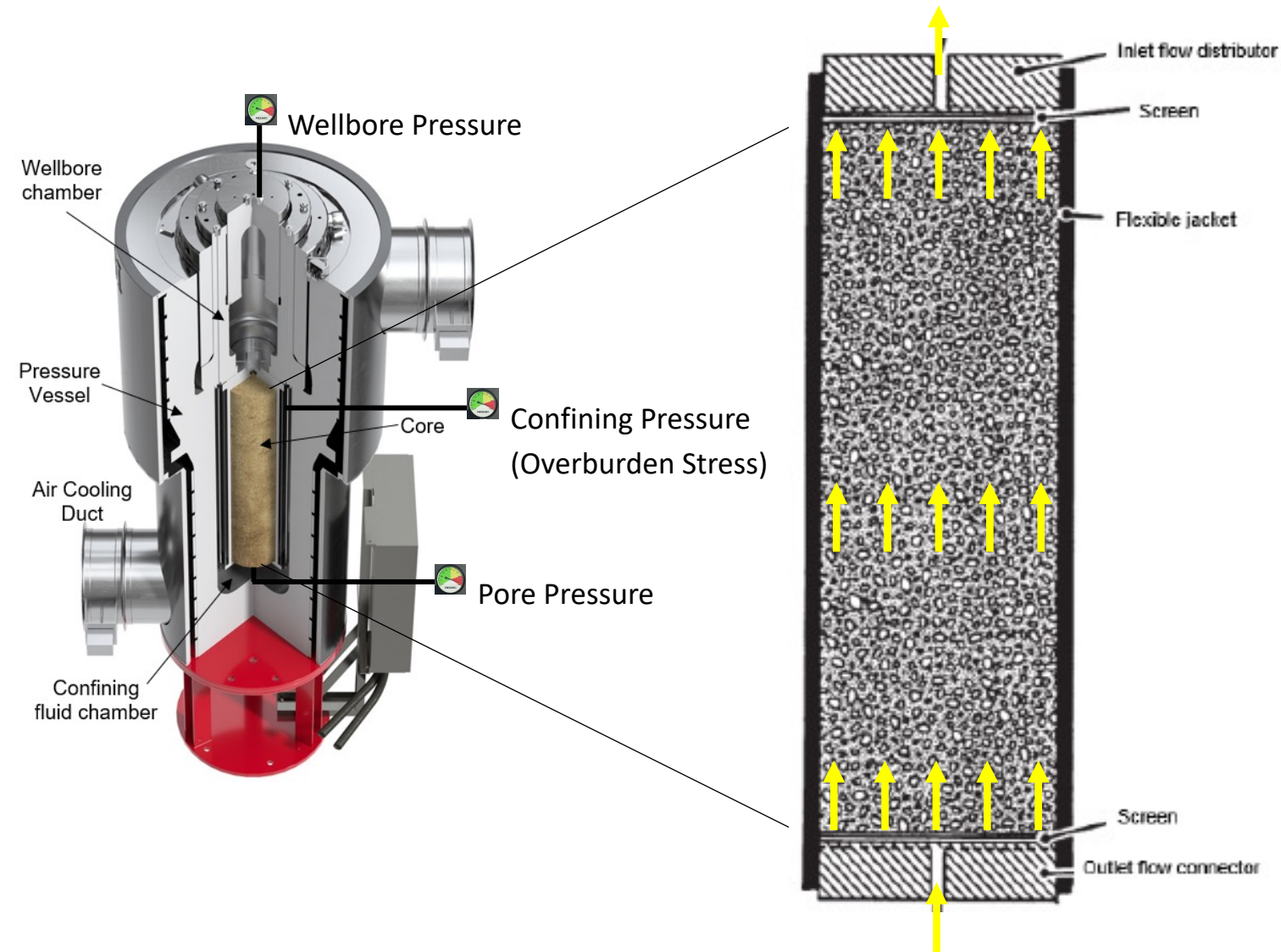
- Viscosity-corrected rate index ( $RI$ ) is then found as:

$$RI = A_1^{-1}$$

- Key Benefit: a systematic approach to determine a single Darcian fluid-independent rate index value.

\*Jones, L. G., Blount, E. M., & Glaze, O. H. (1976). Use of Short Term Multiple Rate Flow Tests To Predict Performance of Wells Having Turbulence. doi:10.2118/6133-MS

- Sandstone core
- Axial pressure/flow configuration
- Production-direction 100% gas flow and 100% liquid flow

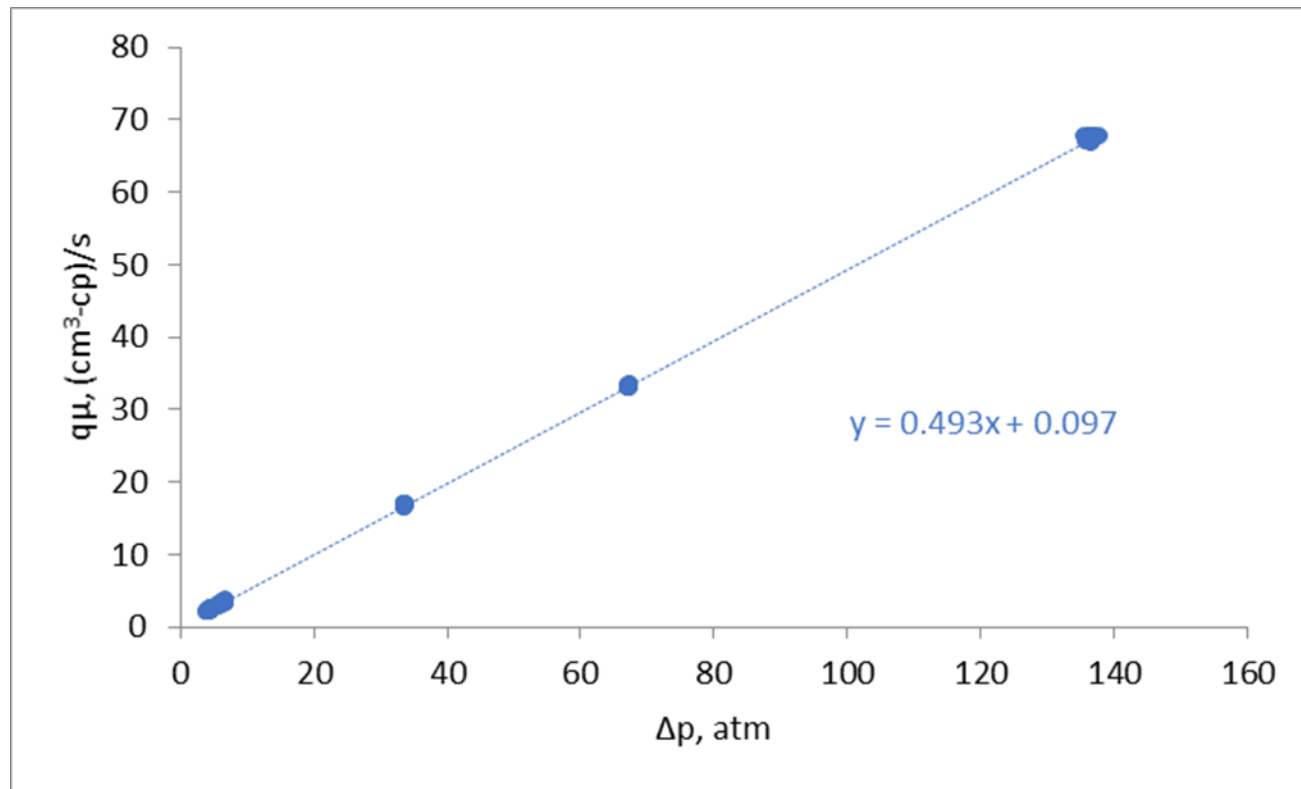


NOTE Not to scale.

Figure 7—Typical Axial-Flow Permeability Equipment

- Liquid Flow

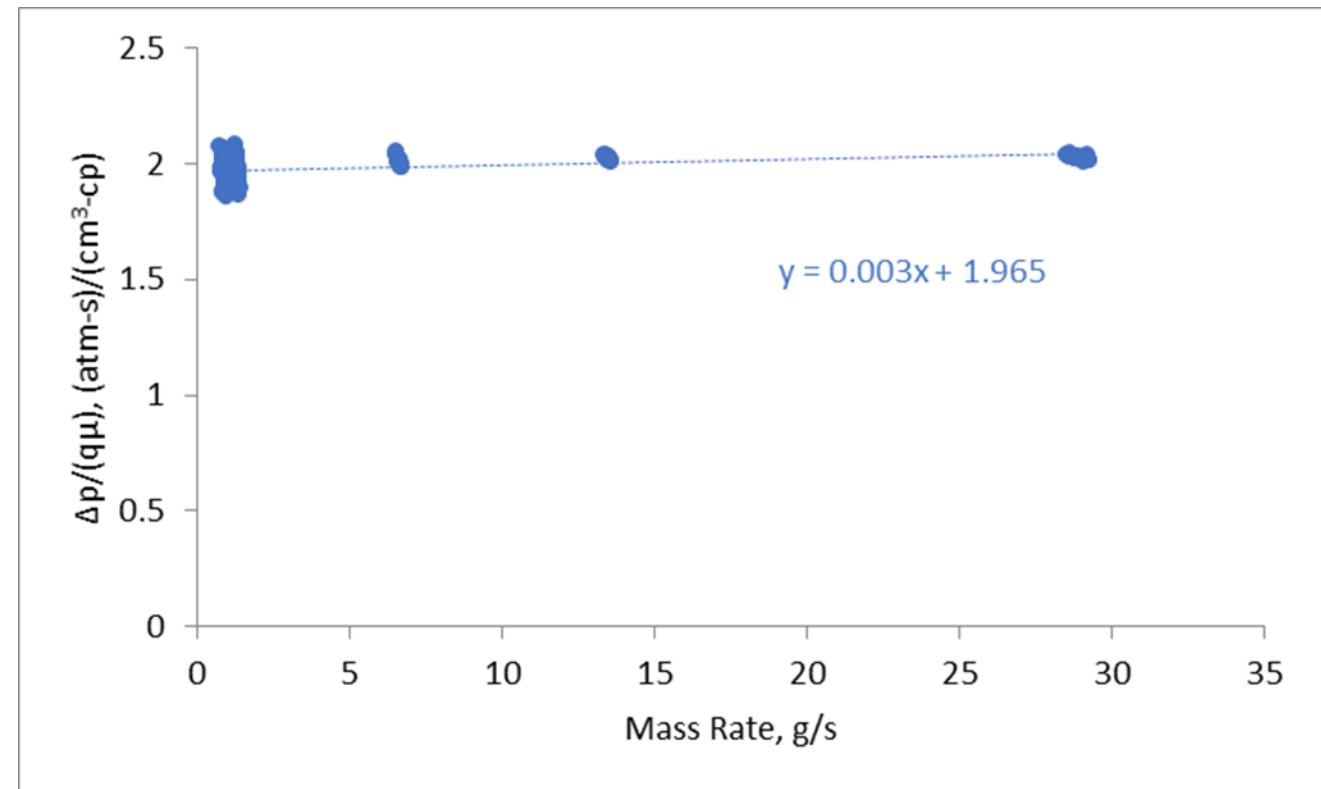
## Conventional Darcy analysis approach



Liquid Flow
$\frac{RI}{(\text{cm}^3 \cdot \text{cp})} \frac{(\text{atm} \cdot \text{s})}{(\text{atm} \cdot \text{s})}$
0.493

- Liquid Flow

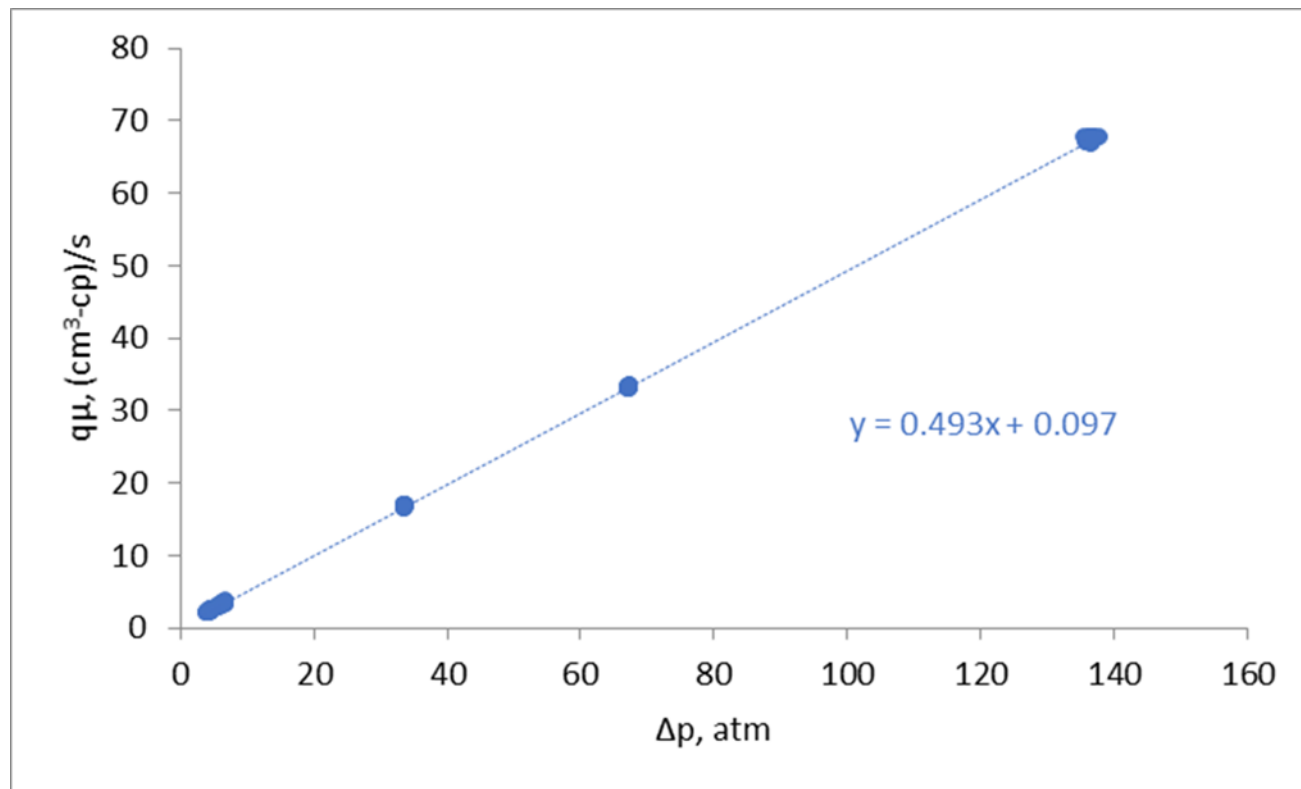
## Viscosity-corrected reciprocal rate index approach



Liquid Flow	
$\frac{A_1}{(\text{atm} \cdot \text{s})} \frac{(\text{cm}^3 \cdot \text{cp})}{(\text{cm}^3 \cdot \text{cp})}$	$\frac{RI}{(\text{cm}^3 \cdot \text{cp})} \frac{(\text{atm} \cdot \text{s})}{(\text{atm} \cdot \text{s})}$
1.965	0.509

- Liquid Flow

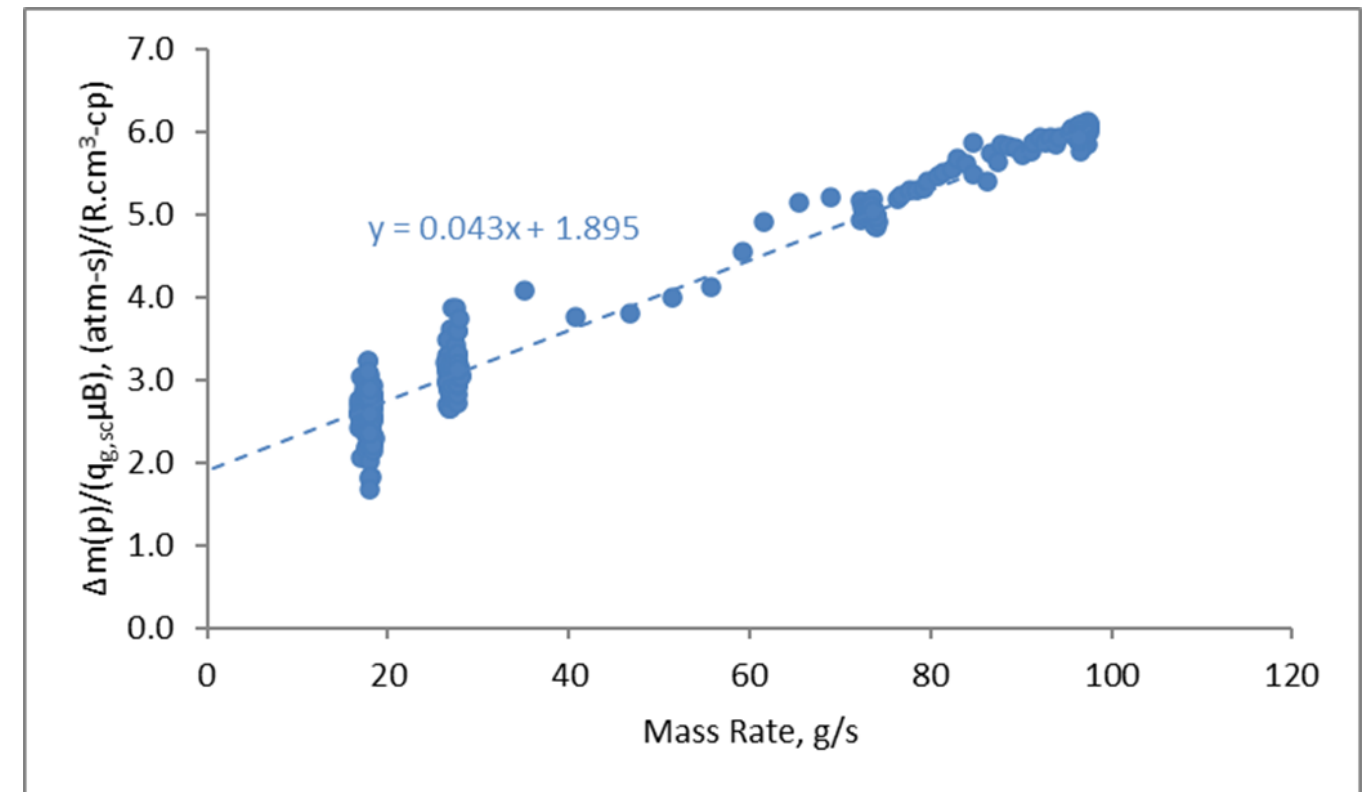
Conventional Darcy analysis approach



Liquid Flow
$\frac{RI}{(\text{cm}^3 \cdot \text{cp})}$ $\frac{(\text{atm} \cdot \text{s})}{(\text{atm} \cdot \text{s})}$
0.493

- Gas Flow

Viscosity-corrected reciprocal rate index approach



Gas Flow	
$\frac{A_1}{(\text{atm} \cdot \text{s})}$ $\frac{(\text{cm}^3 \cdot \text{cp})}{(\text{cm}^3 \cdot \text{cp})}$	$\frac{RI}{(\text{cm}^3 \cdot \text{cp})}$ $\frac{(\text{atm} \cdot \text{s})}{(\text{atm} \cdot \text{s})}$
1.895	0.528



- Sandstone core
- Deep penetrating charge
- Axi-radial pressure/flow configuration
- Production-direction 100% gas flow and 100% liquid flow

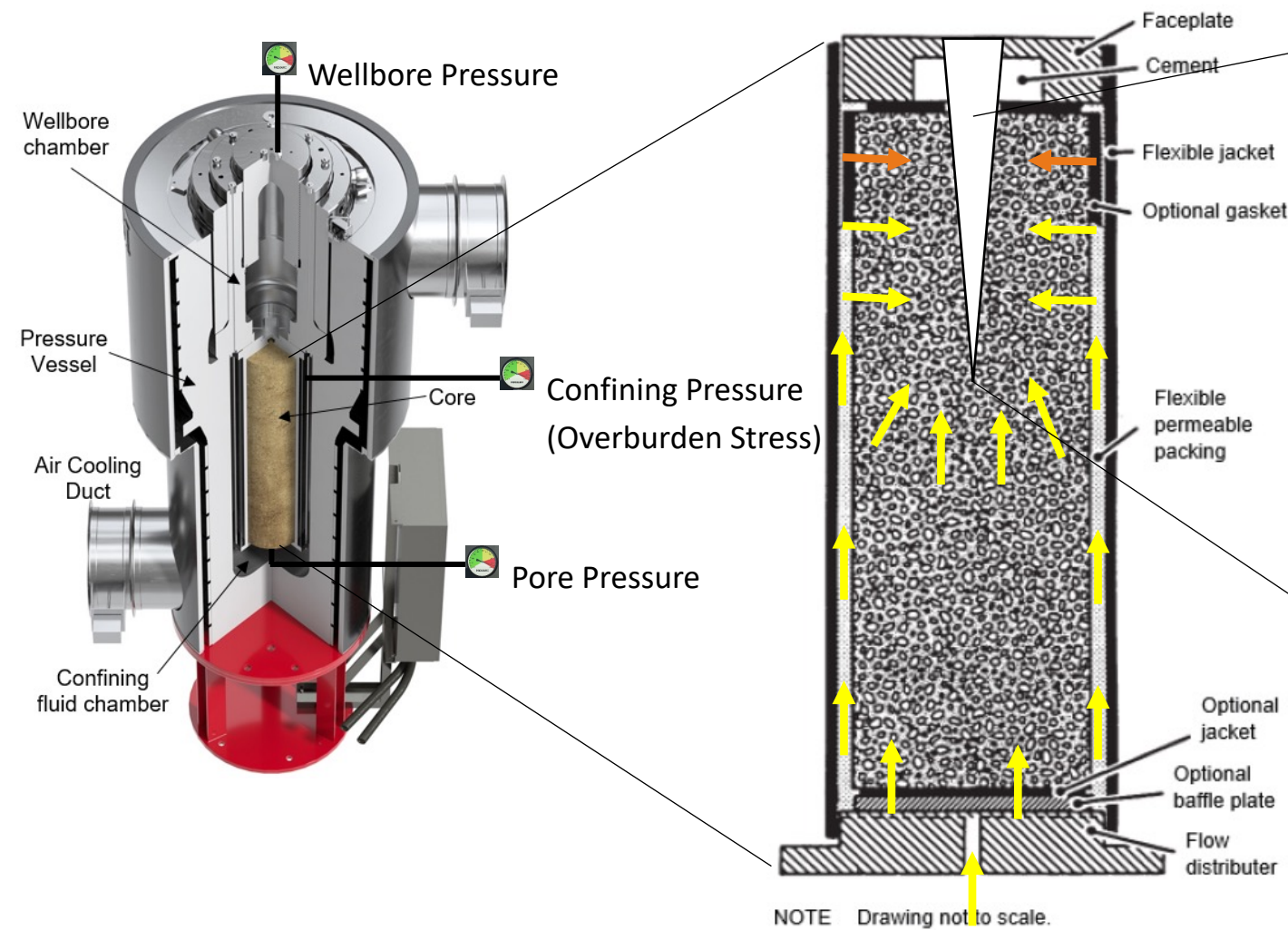
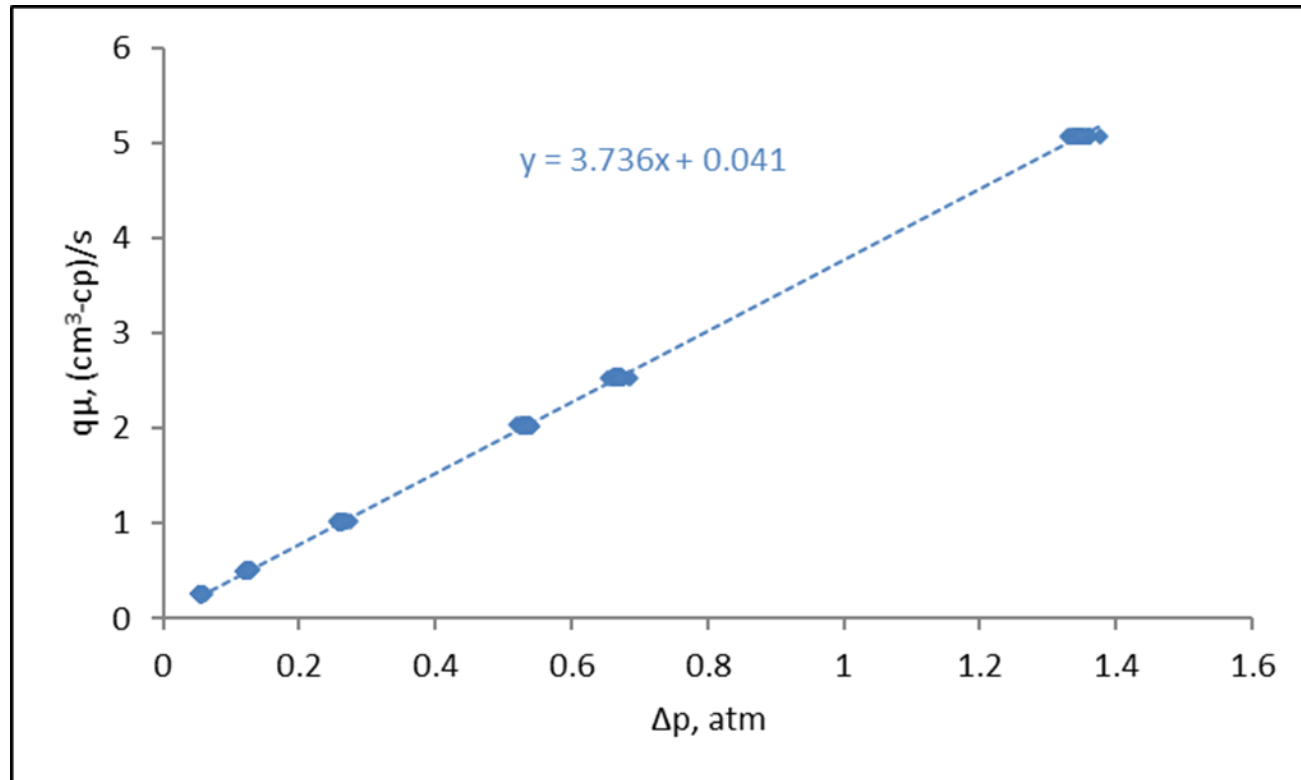


Figure 10—Typical Radial-flow Geometry



- Liquid Flow

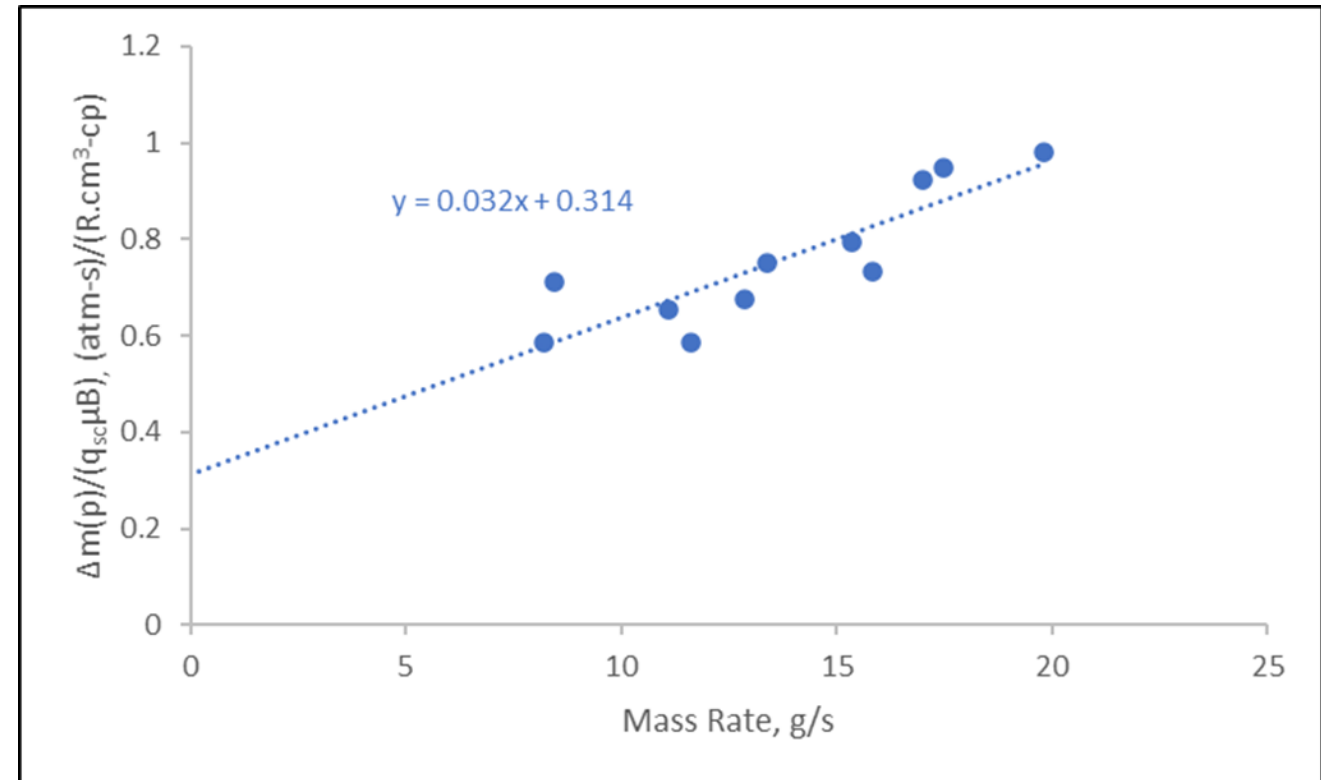
Conventional Darcy analysis approach



Liquid Flow
$\frac{RI}{(\text{cm}^3 \cdot \text{cp})} \frac{(\text{atm} \cdot \text{s})}{(\text{atm} \cdot \text{s})}$
3.736

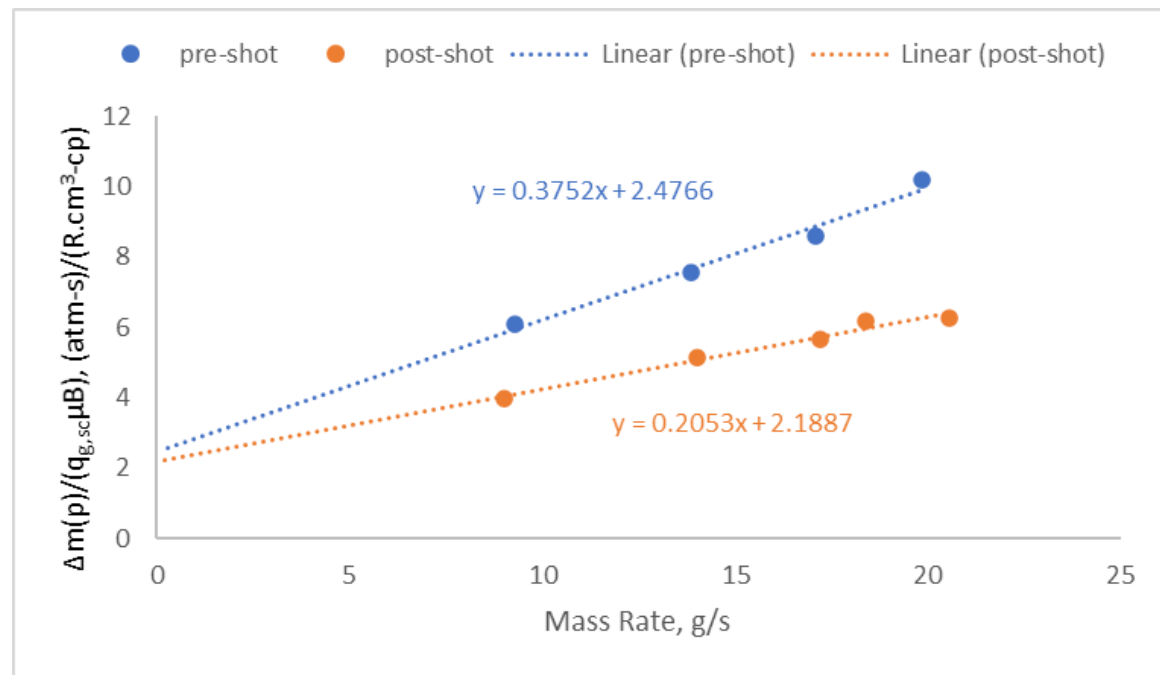
- Gas Flow

Viscosity-corrected reciprocal rate index approach



Gas Flow	
$\frac{A_1}{(\text{atm} \cdot \text{s})} \frac{(\text{cm}^3 \cdot \text{cp})}{(\text{cm}^3 \cdot \text{cp})}$	$\frac{RI}{(\text{cm}^3 \cdot \text{cp})} \frac{(\text{atm} \cdot \text{s})}{(\text{atm} \cdot \text{s})}$
0.314	3.185

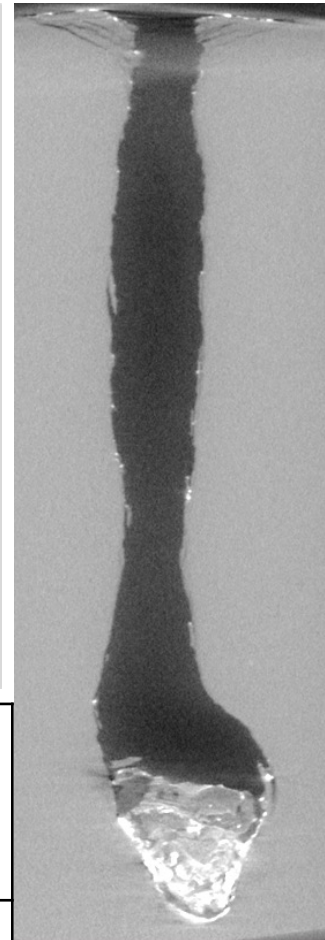
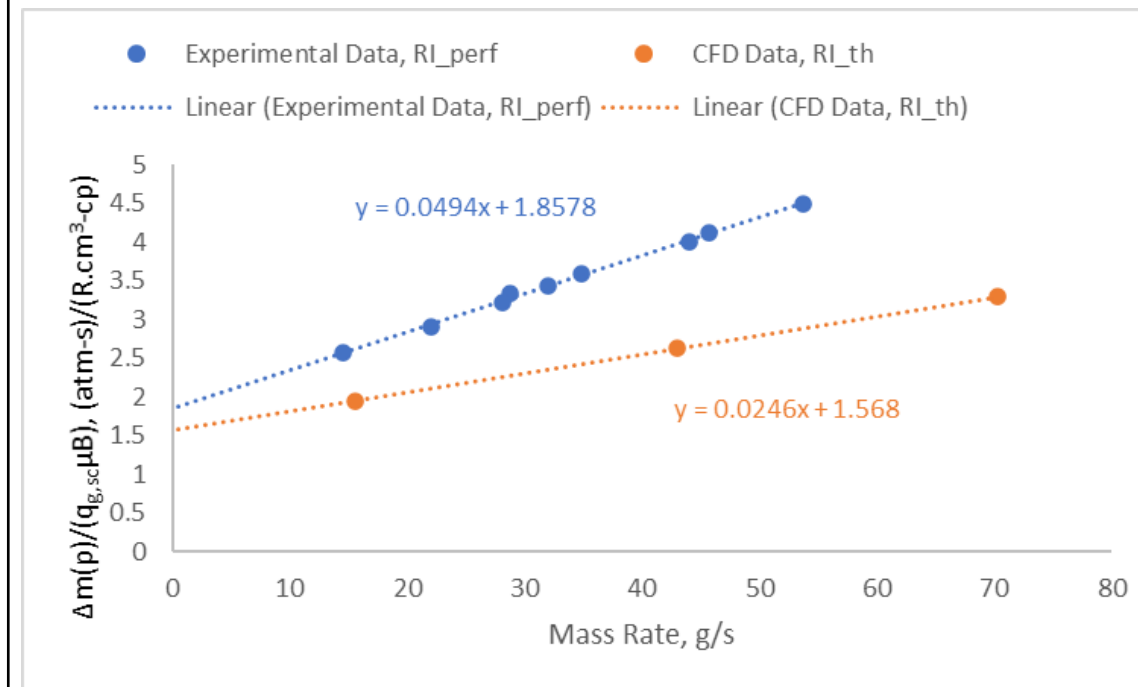
## ■ Axial configuration Test for *RR*:



	$A_1$ $\frac{(\text{atm} \cdot \text{s})}{(\text{cm}^3 \cdot \text{cp})}$	$RI$ $\frac{(\text{cm}^3 \cdot \text{cp})}{(\text{atm} \cdot \text{s})}$
Pre-shot	2.477	0.404
Post-shot	2.189	0.457

$$RR = \frac{RI_{\text{postshot}}}{RI_{\text{preshot}}} = \frac{0.457}{0.404} = 1.132$$

## ■ Axi-radial Configuration Test for *CFE*:



	$A_1$ $\frac{(\text{atm} \cdot \text{s})}{(\text{cm}^3 \cdot \text{cp})}$	$RI$ $\frac{(\text{cm}^3 \cdot \text{cp})}{(\text{atm} \cdot \text{s})}$
Actual	1.858	0.538
Ideal	1.568	0.638

$$CFE = \frac{RI_{\text{actual}}}{RI_{\text{ideal}}} = \frac{0.538}{0.638} = 0.844$$

- This alternative method provides:
  - A systematic approach to determine a single Darcian, fluid- and rate-independent, rate index value. As defined, this rate index is only a function of permeability and flow path (length, area, & geometry).
    - Helpful for when more than one fluid is tested (e.g., liquid injection followed by gas production), when the same fluid is tested but at different temperatures, when different flow rates or differential pressures are tested.
    - Important when determining CFE → single-shot skin → crushed zone permeability.
  - A different perspective of the flow data, which can be helpful in the analysis process of determining the flowing properties of the perforation.

# Q&A

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